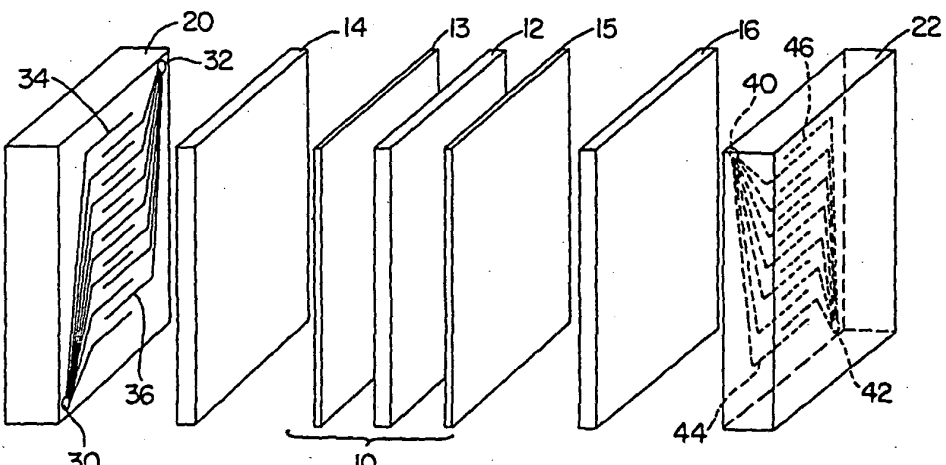


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(21) International Application Number: PCT/US99/21411 (22) International Filing Date: 17 September 1999 (17.09.99) (30) Priority Data: 09/156,714 18 September 1998 (18.09.98) US (71) Applicant: ENERGY PARTNERS, L.C. [US/US]; Technology Center, Suite 102, 1501 Northpoint Parkway, West Palm Beach, FL 33407 (US). (72) Inventors: WYNNE, Robert, Kenneth; 3859 Van Cott Circle, Lake Park, FL 33403 (US). NEUTZLER, Jay, Kevin; 3204 Morning Glory Court #10, Palm Beach Gardens, FL 33410 (US). BARBIR, Frano; 10163 Aspen Way, Palm Beach Gardens, FL 33410 (US). GURAU, Vladimir; 15555 S.W. 83rd Avenue, Miami, FL 33157 (US). PIERCE, Walter, Edward, III; 4960 McConnel Street, Lake Worth, FL 33463 (US). (74) Agents: NELSON, Gregory, A. et al.; Quarles & Brady LLP, 4th floor, 222 Lakeview Avenue, P.O. Box 3188, West Palm Beach, FL 33402-3188 (US).		(81) Designated States: AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, CA, CH, CN, CR, CU, CZ, DE, DK, EE, ES, FI, GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MD, MG, MK, MN, MW, MX, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, SL, TJ, TM, TR, TT, UA, UG, UZ, VN, YU, ZA, ZW, ARIPO patent (GH, GM, KE, LS, MW, SD, SL, SZ, TZ, UG, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, GW, ML, MR, NE, SN, TD, TG). Published <i>With international search report.</i> <i>Before the expiration of the time limit for amending the claims and to be republished in the event of the receipt of amendments.</i>
(54) Title: SELF-HUMIDIFYING FUEL CELL  (57) Abstract <p>A self-humidifying polymer electrolyte membrane (PEM) fuel cell assembly has an ion-exchange membrane (12) interposed between hydrogen and oxygen diffusion layers (14, 16) to form a membrane electrode assembly (MEA) (10). The MEA (10) is in turn interposed between a pair of current collector plates (20, 22) having flow field channels (34, 36) for flowing the reactants adjacent the respective diffusion layers to produce corresponding anodic and cathodic electrochemical reactions. Various embodiments of the assembly incorporate one or more of the following features: interdigitated flow field channels (34, 36), countercurrent reactant flows, opposing channel alignment, and uncatalyzed membrane hydration enhancement zones (82, 84).</p>		

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Summary of the Invention

It is an object of this invention to provide a polymer electrolyte membrane (PEM) fuel cell capable of maintaining membrane hydration upon the introduction of at least one
5 dry reactant stream into the cell.

It is another object of this invention to provide a PEM fuel cell in which membrane hydration is maintained using water provided as a byproduct of electrochemical reactions within the fuel cell.

It is a further object of this invention to provide a PEM fuel cell which does not
10 require components dedicated to pre-humidification of reactant gas streams.

These and other objects of the invention are achieved by the PEM fuel cell assembly of the present invention. A self-humidifying polymer electrolyte membrane (PEM) fuel cell has a membrane electrode assembly (MEA), comprising an ion-exchange membrane interposed between catalyzed anode and cathode electrodes. The MEA is interposed
15 between a pair of gas diffusion backings, and the resulting structure is interposed between fuel and oxidant flow field plates. The fuel flow field plate has a fuel stream inlet, a fuel stream outlet, and means for flowing the fuel stream therebetween. The oxidant flow field plate has an oxidant stream inlet, an oxidant stream outlet, and means for flowing the oxidant stream therebetween.

20 In the preferred embodiment of the invention, fuel and oxidant flows are strategically directed to enhance the transfer of water byproduct, through the ion exchange membrane, between opposing gas streams. Dry fuel and oxidant streams are introduced into respective fuel and oxidant inlets. The corresponding flow field plate channels are oriented such that dry portions of reactant stream adjacent to one surface of the membrane
25 generally oppose hydrated portions of reactant stream on the opposite surface of the membrane. In this embodiment, membrane hydration is maximized by providing countercurrent reactant flows. In other words, the reactant gases are directed in generally opposing directions through the fuel cell. Preferably, opposing channel lengths having disparate humidification levels are aligned to provide an increased humidification gradient therebetween, resulting in enhanced mass transfer of water across the membrane in the
30 direction of the less humidified reactant stream. Channel alignment also minimizes the

One commonly-used method for pre-humidifying fuel cell gas streams is to employ membrane-based humidifiers. Where membrane-based humidifiers are employed, reactant humidification is achieved by flowing the respective gases on one side of a water vapor exchange membrane while flowing deionized water on the opposite side of the membrane.

5 In such arrangements, water is transported across the membrane to humidify the fuel and oxidant gases. Another known technique for pre-humidifying the reactant gas streams comprises exposing the gases directly to water in an evaporation chamber to permit the gas to absorb evaporated water. Yet another known pre-humidification technique comprises directly injecting or aspirating water into the respective gas streams before introducing
10 them into the fuel cell.

Generally, pre-humidification is undesirable because it requires auxiliary fuel cell components, increasing the relative complexity of fuel cell systems. For instance, pre-humidification generally requires dedicated components for storing and transporting water. Additional components may also present system reliability issues. For example, where fuel
15 cells are operated in sub-freezing conditions, water solidification can result in the weakening of mechanical components. Auxiliary water storage and transport components also reduce operating efficiency and add to the overall cost of the system.

For the foregoing reasons, the need exists for a PEM fuel cell assembly capable of maintaining hydration of the fuel cell membrane without requiring additional components
20 for humidifying reactant streams prior to their introduction into the fuel cell stack.

Brief Description of the Drawings

Fig. 1 is an exploded view of a PEM fuel cell assembly in accordance with the present invention;

5 Fig. 2 is a cross-sectional view of a PEM fuel cell assembly having interdigitated flow field channels in accordance with a preferred embodiment of the present invention;

Fig. 3 is a front view of a field flow plate having an interdigitated reactant flow channel design in accordance with a preferred embodiment of the present invention;

10 Fig. 4 is a schematic of a preferred fuel cell assembly in which opposing collector plate channels are shown superimposed on one another;

Fig. 5 is a schematic of a fuel cell assembly having membrane hydration enhancement zones in accordance with an alternate embodiment of the present invention;

Fig. 6 is a schematic of a fuel cell assembly having membrane hydration enhancement zones in accordance with a further embodiment of the present invention;

15 Fig. 7 is a schematic of a fuel cell assembly incorporating double-interdigitated flow field channels, in which opposing collector plate channels are shown superimposed on one another, in accordance with an alternate embodiment of the invention;

20 Fig. 8 is a graph illustrating the effect of air flow rate and humidification level on the performance of a fuel cell assembly constructed in accordance with the present invention;

Fig. 9 is a graph illustrating the effect of humidification level on the performance of a fuel cell assembly constructed in accordance with the present invention.

water transfer distance between opposing channels. At one extreme, portions of channels carrying dry reactant oppose portions of channels on the opposite side of the membrane carrying saturated reactant.

Although contiguous channel designs (e.g., serpentine patterns) are effective, it is preferred that noncontiguous, interdigitated channels are employed to provide forced convection of the reactants through the respective fuel and oxidant diffusion layers. Forced convection propels the reactants closer to the respective catalyst layers, thereby enhancing the electrochemical reactions at the opposing cathode and anode sides of the membrane. As a result, the rate of production of water byproduct at the cathode is increased. Furthermore, although countercurrent flows are preferred, other orientations have proven effective. For example, perpendicular interdigitated flow fields, resulting in reactant cross flow, are effective for enhancing membrane hydration in fuel cells employing at least one dry reactant stream.

In an alternate embodiment of the invention, liquid-to-gas humidification is accomplished by directing dry fuel and oxidant inlet flow streams over liquid deionized water zones prior to their introduction into catalyzed regions of the cell. In particular, a stream of deionized water is directed over one side of an uncatalyzed portion of membrane, while dry reactant gas is directed on the opposite side of the membrane. The water is transported through the bare membrane and diffuses into the inlet gas stream as water vapor.

In a further embodiment of the invention, membrane hydration enhancement zones are incorporated to provide additional membrane hydration / gas stream humidification. In particular, the zones comprise uncatalyzed areas of the PEM. These regions may consist of bare membrane interposed between gas diffusion layers or, alternatively, bare membrane directly interposed between opposing flow field plates. Uncatalyzed membrane is less hydrophobic than catalyzed membrane. Consequently, liquid water is more apt to be absorbed into uncatalyzed areas of the membrane. Absorption of liquid water into uncatalyzed regions of the membrane is further aided by the elimination of exothermic electrochemical reactions which normally occur at catalyzed membrane/diffusion layer interfaces. By eliminating this reaction heat, the membrane within the zone is maintained at a reduced temperature and is less prone to drying.

interdigitated flow channels on the cathode (oxidant) side operate in a similar manner. As a result of the enhanced electrochemical reactions, the production rate of water byproduct at the cathode is increased. A portion of the additional water produced at the cathode back-diffuses through the membrane toward the anode. Consequently, the availability of water at the anode is also increased when interdigitated channels are used.

Referring briefly to FIG. 3, a front view of flow field plate 20 is depicted to illustrate a unique interdigitated flow field pattern in accordance with the preferred embodiment of the present invention. Conventional interdigitated designs typically employ a plurality of flow channels branching off from a main flow channel, e.g., see U.S. Pat. No. 5,641,586 to Wilson. In contrast, the present invention employs non-overlapping flow channels 34, 36 each extending from a reactant stream port 30, 32. The interdigitated flow pattern of the present invention results in more uniform fluid flow distribution, reduced channel moisture retention, and decreased channel pressure drop. Consequently, more uniform electrical current density is achieved across the fuel cell.

Referring now to FIG. 4, the fuel and oxidant flow field plate channels are shown superimposed for the purpose of discussion. In the preferred embodiment of the present invention, the fuel and oxidant flow fields are oriented to achieve countercurrent fuel and oxidant flow streams. In other words, the fuel and oxidant streams flow in generally opposed directions across the fuel cell assembly. The water content of both the fuel and oxidant streams increases in the flow direction of the respective reactant through the fuel cell. Therefore, by employing a countercurrent flow arrangement, the region of the anode layer with the highest water content substantially coincides with the region of the cathode layer having the lowest water content, and vice versa. As a result, countercurrent reactant flow streams result in more uniform hydration of the ion-exchange membrane.

Fuel and oxidant inlet ports are denoted by reference numerals 30 and 42, respectively. Fuel and oxidant outlet ports are denoted by reference numerals 32 and 40, respectively. The horizontal lengths of the corresponding fuel and oxidant channels are shown slightly offset from one another in a vertical direction for illustrative purposes; although such an arrangement is possible, it is not preferred. Preferably, the horizontal lengths of fuel inlet channels 34 and oxidant outlet channels 44, and the horizontal lengths of oxidant inlet channels 46 and fuel outlet channels 36, overlies one another when viewed

Detailed Description of the Preferred Embodiments

Referring now to FIGS. 1 and 2, a polymer electrolyte membrane (PEM) fuel cell includes a membrane electrode assembly (MEA) 10, gas diffusion backings 14, 16, and current collector / reactant flow field plates 20, 22. Membrane electrode assembly 10 consists of a polymer electrolyte membrane 12 interposed between a pair of electrodes 13, 15. The electrodes include a catalyst, such as platinum or platinum supported on carbon, for inducing desired electrochemical reactions. The catalyst can be attached to the diffusion backings 14, 16, and the backings subsequently pressed against the membrane 12. However, it is preferred that the catalyst is directly adhered to the membrane. Membrane electrode assembly 10 is interposed between porous, electrically-conductive gas diffusion backings 14 and 16. Examples of gas diffusion backings include carbon/graphite fiber paper and carbon/graphite cloth sheets. Fuel and oxidant flow field plates 20 and 22 are positioned on opposing anode and cathode sides of the assembly, respectively. In operation, multiple fuel cell assemblies are positioned side by side to form a fuel cell stack (not shown).

Fuel flow field plate 20 has fuel inlet channels 34 extending from fuel inlet port 30, and fuel outlet channels 36 extending from fuel outlet port 32. Similarly, oxidant flow field plate 22 has oxidant inlet channels 46 extending from oxidant inlet port 42, and oxidant outlet channels 44 extending from oxidant outlet port 40. The respective inlet and outlet channels formed in each plate are noncontiguous, or dead-ended, and interdigitated. By employing dead-ended, interdigitated inlet and outlet channels, the reactants are forced to flow through the respective porous electrodes 14, 16. For instance, referring to fuel flow field plate 20 on the anode side of the fuel cell, hydrogen gas entering through fuel inlet port 30 and filling inlet channels 34 is forced through porous diffusion layer 14 before continuing to flow through fuel outlet channels 36 toward fuel outlet 32. Conventional contiguous channel designs, such as those employing serpentine patterns, rely primarily on diffusion for fluid transport through the diffusion layer. In contrast, the interdigitated channels of the present invention employ forced convection of the reactant through the diffusion layer, urging the reactant closer to the catalyst layer. Forced convection results in more rapid reactant flow through the diffusion layer vis-a-vis diffusion. As a result, the electrochemical reaction rates at the respective catalyst sites are increased. The

membrane. This results in both local membrane hydration and increased humidification of the reactant stream flowing on the opposite side of the membrane. Lateral absorption of water through the membrane results in increased hydration of catalyzed regions of the membrane as well.

5 Membrane hydration is further enhanced by the lack of electrochemical reactions in these hydration enhancement zones. As previously described, the fuel cell electrochemical reactions at the respective electrodes are initiated by catalyst layers at the membrane/diffusion layer interfaces. The heat produced by these electrochemical reactions tends to dry the membrane locally. However, absent a catalyst, the gas reactants flow
10 without producing these exothermic electrochemical reactions. The reduced membrane temperatures decrease local membrane dehydration.

 Preferably, uncatalyzed areas 82 and 84 are strategically located proximate to reactant flow inlet and outlet areas on opposite sides of catalyzed area 80. Since reactant humidification typically increases in the reactant flow direction, the lowest reactant
15 humidification levels typically occur near the reactant channel inlets, and the highest reactant humidification levels typically occur near the reactant channel outlets. At least a portion of the humidified outlet channel lengths are routed through the humidification zones 82, 84, hydrating the membrane locally through absorption of reactant stream water. Inlet channels carrying dry reactant gas are routed through the humidification zones 82, 84 on
20 the opposite side of the membrane. The humidification gradient across the membrane, caused by the opposing dry and humidified reactant streams, results in the transfer of water absorbed by the membrane to the respective dry inlet gas streams.

 Humidification zones may be created by utilizing an ion-exchange membrane with integrally attached electrodes that maintain uncatalyzed regions. Alternatively,
25 humidification zones may be created by providing a diffusion layer having both catalyzed and uncatalyzed areas. In some instances, it may be desirable to further treat the diffusion layer such that the catalyzed areas are hydrophobic, and the uncatalyzed areas, corresponding to humidification zones, are hydrophilic. This is easily accomplished by selectively coating the diffusion layer with a hydrophobic material such as Teflon®.
30 Alternatively, humidification zones can comprise an ion-exchange membrane directly interposed between opposing flow field plates, where one or both sides of the membrane

perpendicular to the reactant flow planes. As used herein, the term "superposed" is used to describe this overlapping relationship of opposing collector plate channels. There are a number of advantages to providing superposed channels. For instance, channel alignment results in corresponding alignment of lands, or non-channel areas, of opposing flow field plate surfaces. Maximizing land-to-land alignment between flow field plates results in optimized electrical conductivity between opposing current collector plates upon compression of the individual cells making up the fuel cell stack. In other words, aligning the opposing collector plate lands minimizes increases in electrical resistance across the cell associated with land-to-channel alignment. Furthermore, channel alignment increases the mass transfer rate of water across the membrane, especially in regions where a well-hydrated gas stream is positioned opposite a dry, or non-hydrated, gas stream. Where this is the case, the water transfer rate across the membrane is increased due to the gradient created by the hydration level differential on opposite sides of the membrane. Channel alignment is especially beneficial for hydrating peripheral regions of the membrane, where dry gases are typically introduced into the cell. Employing the preferred countercurrent reactant flow arrangement, the ingress of dry reactant gas on one side of the membrane is aligned with the egress of well-hydrated reactant gas on the opposite side of the membrane. In conventional fuel cell assemblies, inlet gas streams are pre-humidified to prevent dehydration of the membrane at gas inlet areas. In the present invention, humidified reactant streams may be provided initially when membranes are completely dry, to initiate the required electrochemical reactions at the respective electrodes. However, upon achieving an adequate fuel cell operating level, adequate membrane hydration can be maintained running only dry reactant flows.

Referring now to FIG. 5, an alternate embodiment of the present invention incorporates at least one membrane hydration enhancement zone. Specifically, portions 82, 84 of the ion-exchange membrane are left uncatalyzed to enhance self-humidification of the fuel cell assembly, especially in regions of the membrane prone to drying. Uncatalyzed membrane areas are less hydrophobic than catalyzed membrane areas. Consequently, uncatalyzed areas are more apt to attract and retain liquid water. Accordingly, as a reactant stream containing liquid water flows through an uncatalyzed region of the membrane, the water is more likely to pool atop, and subsequently absorb into, the

convection, from inlet channels 52, through intermediate channels 54, to outlet channels 56. As a result of the double convection, both reactant and water vapor are more evenly distributed during transport across the polymer electrolyte membrane. This embodiment may further incorporate features of previously described embodiments, e.g., countercurrent reactant flow, superposed channels, etc.

While the preferred embodiments of the invention have been illustrated and described, it will be clear that the invention is not so limited. Numerous modifications, changes, variations, substitutions and equivalents will occur to those skilled in the art without departing from the spirit and scope of the present invention as described in the claims.

are not supported by a diffusion layer. In this embodiment, it is preferable to use an integrally reinforced PEM membrane, such as GORE PRIMEA®, manufactured by W.L. Gore & Associates, Inc. of Elkton, Maryland. Elimination of the diffusion layer reduces gas flow and permits localized "pooling" of water. The elimination of the diffusion layer also permits gas-to-water sealing along the periphery of the zone. These water-to-membrane contact zones may directly humidify a gas flowing on the opposite side of the membrane, or extend sealed deionized water zones via lateral water absorption/hydration through the membrane. Hydration enhancement zones 86 may be distributed throughout the fuel cell assembly for further membrane hydration. Although specific humidification zone quantities and geometries are illustrated, the invention is not intended to be so limited. For instance, the membrane can incorporate hundreds, or even thousands, of uncatalyzed areas (e.g., microdots), having dimensions on the order of microns, distributed throughout the assembly to enhance membrane hydration.

Referring now to FIG. 6, in a further embodiment of the invention, liquid-to-gas membrane hydration / reactant humidification is enhanced by directing dry fuel and oxidant inlet flow streams over liquid deionized water zones prior to their introduction into catalyzed regions of the cell. In particular, a stream of deionized water introduced into the fuel cell assembly is directed over one side of an uncatalyzed portion of membrane, while dry reactant gas is directed over the opposite side of the membrane. Water absorbed by, and transported through, the bare membrane diffuses into the dry inlet gas stream as water vapor.

Referring now to FIG. 7, yet a further embodiment of the invention incorporates a double-interdigitated flow field channel design. The cathode and anode flow field channels are shown superimposed and slightly offset. The vertical offset is for illustrative purposes only and is not preferred. The fuel cell assembly has at least one uncatalyzed humidification zone and at least one catalyzed reaction zone. In operation, two reactants are communicated through the assembly. However, for simplicity, the following description only refers to one of the reactants. A first reactant is introduced through inlet 50 into inlet channels 52. Inlet channels 52 extend across the humidification zone, and function solely to humidify the first reactant. Preferably, the first reactant is humidified to the point of saturation. The saturated first reactant is subsequently transferred, by forced

flowing an oxidant stream both comprise interdigitated inlet and outlet flow field channels, said oxidant inlet channels and fuel outlet channels, and said oxidant outlet channels and fuel inlet channels, at least partially superposed across said ion-exchange membrane to enhance channel-to-channel water transfer across said membrane.

5

6. A self-humidifying polymer electrolyte membrane (PEM) fuel cell assembly as recited in claim 1, further comprising at least one membrane hydration enhancement zone.

10 7. A self-humidifying polymer electrolyte membrane (PEM) fuel cell assembly as recited in claim 6, wherein said at least one membrane hydration enhancement zone comprises an uncatalyzed area of said membrane interposed between gas diffusion layers.

8. A self-humidifying polymer electrolyte membrane (PEM) fuel cell assembly as recited in claim 7, wherein at least one of said gas diffusion layers is hydrophilic.

15

9. A self-humidifying polymer electrolyte membrane (PEM) fuel cell assembly as recited in claim 6, wherein at least one surface of said membrane is directly adjacent to a flow field plate surface.

20 10. A self-humidifying polymer electrolyte membrane (PEM) fuel cell assembly as recited in claim 6, wherein said at least one membrane hydration enhancement zone comprises a plurality of membrane hydration zones dispersed throughout said fuel cell assembly.

25 11. A self-humidifying polymer electrolyte membrane (PEM) fuel cell assembly as recited in claim 6, wherein said at least one membrane hydration enhancement zone comprises deionized water and gas reactant streams directed over opposite sides of said ion-exchange membrane.

We claim:

1. A self-humidifying polymer electrolyte membrane (PEM) fuel cell assembly having an ion-exchange membrane interposed between a pair of electrodes to form a membrane/electrode assembly (MEA), the MEA interposed between fuel and oxidant diffusion layers, the fuel cell assembly comprising:
 - a fuel flow field plate having a fuel stream inlet, a fuel stream outlet, and means for flowing a fuel stream therebetween; and
 - an oxidant flow field plate having an oxidant stream inlet, an oxidant stream outlet, and means for flowing an oxidant stream therebetween, said oxidant and fuel streams having countercurrent stream flows, at least one of said means for flowing a fuel stream and said means for flowing an oxidant stream employing forced convection of said stream through one of said diffusion layers.
2. A self-humidifying polymer electrolyte membrane (PEM) fuel cell assembly as recited in claim 1, wherein at least one of said means for flowing a fuel stream and said means for flowing an oxidant stream comprises interdigitated flow field plate channels.
3. A self-humidifying polymer electrolyte membrane (PEM) fuel cell assembly as recited in claim 2, wherein said interdigitated flow field plate channels comprise a first plurality of non-overlapping inlet channels extending from a common reactant stream inlet port, and a second plurality of non-overlapping outlet channels extending from a common reactant stream outlet port.
4. A self-humidifying polymer electrolyte membrane (PEM) fuel cell assembly as recited in claim 1, wherein said means for flowing a fuel stream and said means for flowing an oxidant stream are at least partially superposed across said ion-exchange membrane to enhance water transfer therebetween.
5. A self-humidifying polymer electrolyte membrane (PEM) fuel cell assembly as recited in claim 2, wherein said means for flowing a fuel stream and said means for

18. A self-humidifying polymer electrolyte membrane (PEM) fuel cell assembly as recited in claim 16, wherein said fuel and oxidant reactants flows have countercurrent flow directions through said membrane hydration enhancement zone.

5 19. A self-humidifying polymer electrolyte membrane (PEM) fuel cell assembly as recited in claim 14, wherein at least one of said means for flowing reactant comprises interdigitated flow field channels.

10 20. A self-humidifying polymer electrolyte membrane (PEM) fuel cell assembly as recited in claim 14, wherein at least one of said means for flowing reactant comprises double-interdigitated flow field channels.

15 21. A method for maintaining membrane hydration in a polymer electrolyte membrane (PEM) fuel cell, the fuel cell having a membrane electrode assembly (MEA) interposed between gas diffusion layers, the gas diffusion layers interposed between fuel and oxidant flow field plates, the method comprising the steps of:
 introducing fuel and oxidant reactants into said fuel cell through respective fuel and oxidant inlets, at least one of said reactants introduced in a dry, nonhumidified state;
 communicating said fuel and oxidant reactants through respective fuel and oxidant
20 flow field channels; and
 exhausting said reactants through fuel and oxidant outlets.

25 22. A method as recited in claim 21, further comprising, prior to the step of exhausting, the step of directing at least one of said reactants through a membrane hydration enhancement zone.

 23. A method as recited in claim 21, wherein said reactants are communicated in countercurrent directions through said fuel and oxidant flow field channels.

30 24. A method as recited in claim 22, wherein said reactants are communicated in countercurrent directions through said fuel and oxidant flow field channels.

12. A self-humidifying polymer electrolyte membrane (PEM) fuel cell assembly as recited in claim 11, wherein said water and gas reactant streams have opposing flow directions.

5 13. A self-humidifying polymer electrolyte membrane (PEM) fuel cell assembly as recited in claim 1, wherein said fuel comprises hydrogen gas.

10 14. A self-humidifying polymer electrolyte membrane (PEM) fuel cell assembly having a membrane/electrode assembly (MEA), the MEA including an ion-exchange membrane interposed between a pair of electrodes, the MEA interposed between a pair of gas diffusion layers, the fuel cell comprising:

 a fuel flow field plate having a fuel stream inlet, a fuel stream outlet, and means for flowing a fuel stream therebetween;

15 an oxidant flow field plate having an oxidant stream inlet, an oxidant stream outlet, and means for flowing an oxidant stream therebetween; and

 at least one membrane hydration enhancement zone.

20 15. A self-humidifying polymer electrolyte membrane (PEM) fuel cell assembly as recited in claim 14, wherein said at least one membrane hydration enhancement zone comprises an uncatalyzed area of said membrane.

25 16. A self-humidifying polymer electrolyte membrane (PEM) fuel cell assembly as recited in claim 14, wherein at least one of said means for flowing is directed through said at least one membrane hydration enhancement zone.

30 17. A self-humidifying polymer electrolyte membrane (PEM) fuel cell assembly as recited in claim 16, wherein the oxidant and fuel reactant stream flows are strategically directed thorough said at least one membrane hydration enhancement zone to maximize water vapor transfer between said reactant stream flows.

INTERNATIONAL SEARCH REPORT

International application No.

PCT/US99/21411

A. CLASSIFICATION OF SUBJECT MATTER

IPC(6) :H01M 8/04, 2/00

US CL :429/13, 30, 34, 38, 39, 40, 46

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

U.S. : 429/13, 30, 34, 38, 39, 40, 46

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

EAST

search terms: flow field plate, flow plate, countercurrent, interdigitated, humidify, hydrate

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	US 5,300,370 A (WASHINGTON et al.) 5 April 1994, col. 3, lines 16-60; col. 8, lines 50-67; col. 12, line 67 to col. 13, line 41; Figs. 1, 2, 5, 9.	14, 16, 17, 19-22, 25, 26, 28, 29 ----- 1-13, 15, 18, 23, 24, 27
Y		
Y	US 5,773,160 A (WILKINSON et al.) 30 June 1998, col. 2, lines 39-58; col. 4, line 52 to col. 5, line 14; col. 6, lines 56-67; Figs. 9, 10.	1, 3, 4, 5, 12, 17, 18, 23, 24
Y	US 5,472,799 A (WATANABE) 5 December 1995, col. 4, lines 44-49, Figs. 2, 3.	7, 10, 15
Y	US 5,108,849 A (WATKINS et al.) 28 April 1992, col. 4, lines 11-18, Fig. 1.	9



Further documents are listed in the continuation of Box C.



See patent family annex.

* Special categories of cited documents:	*T* later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
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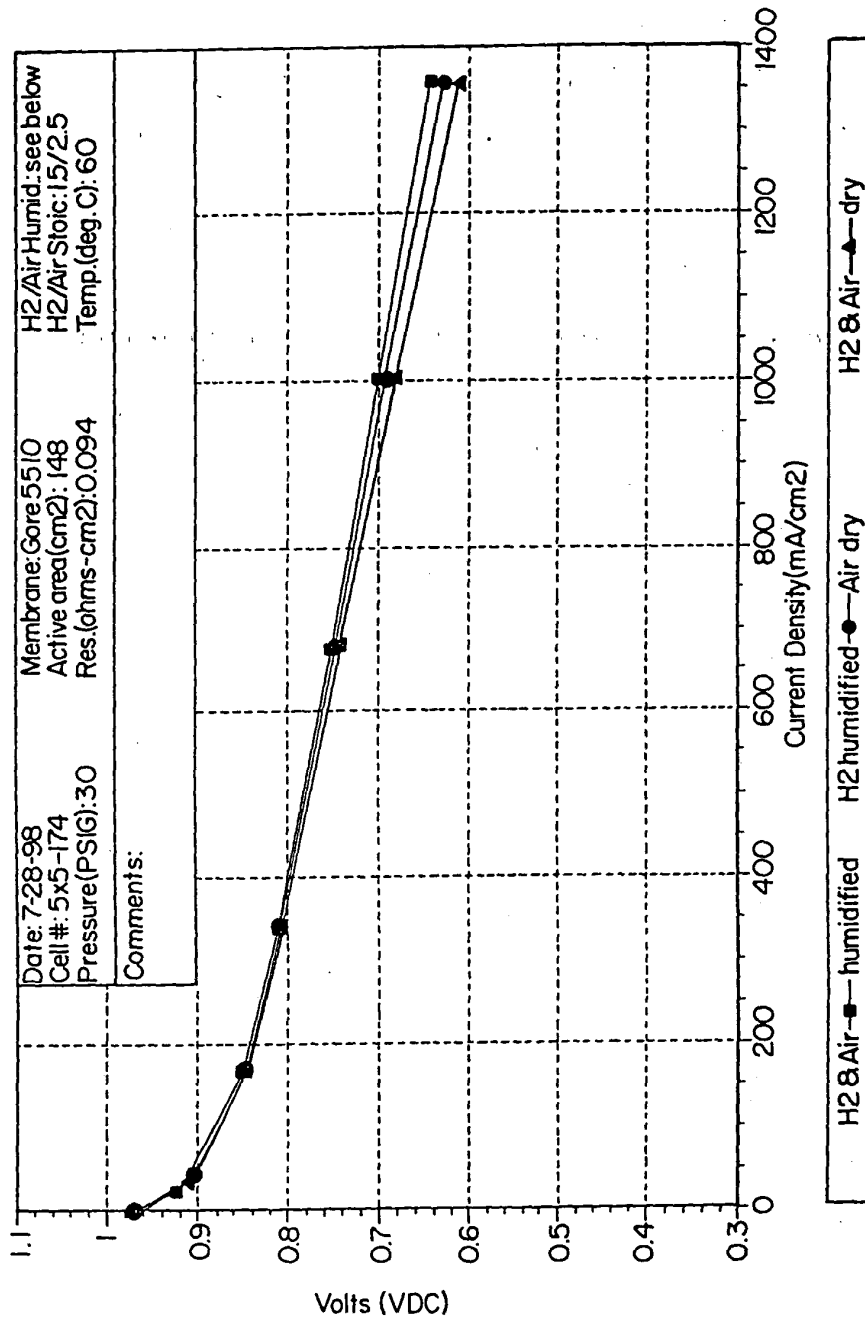


FIG. 9

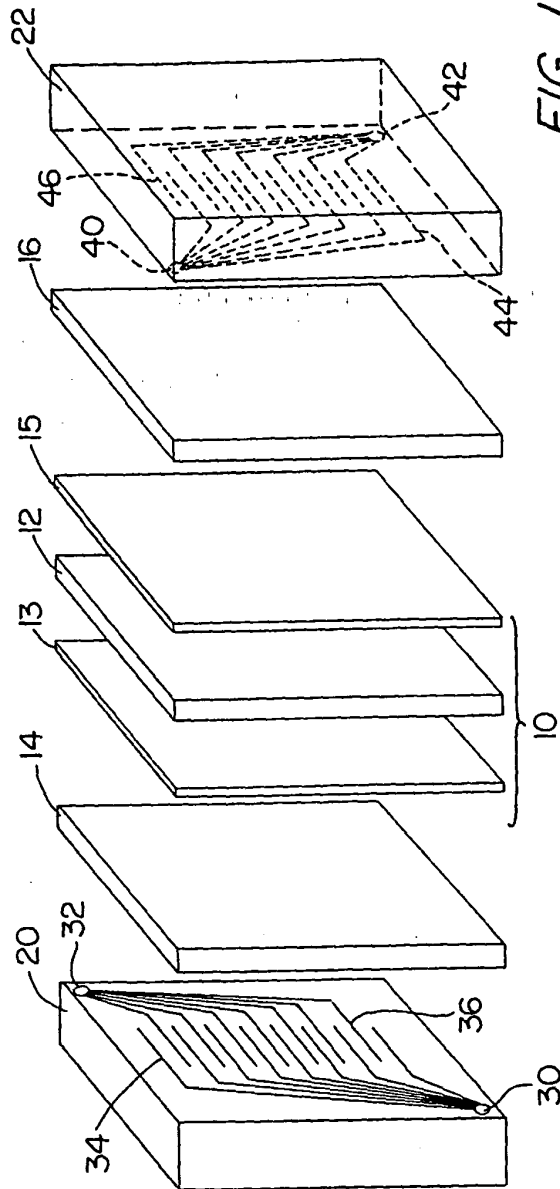


FIG. 1

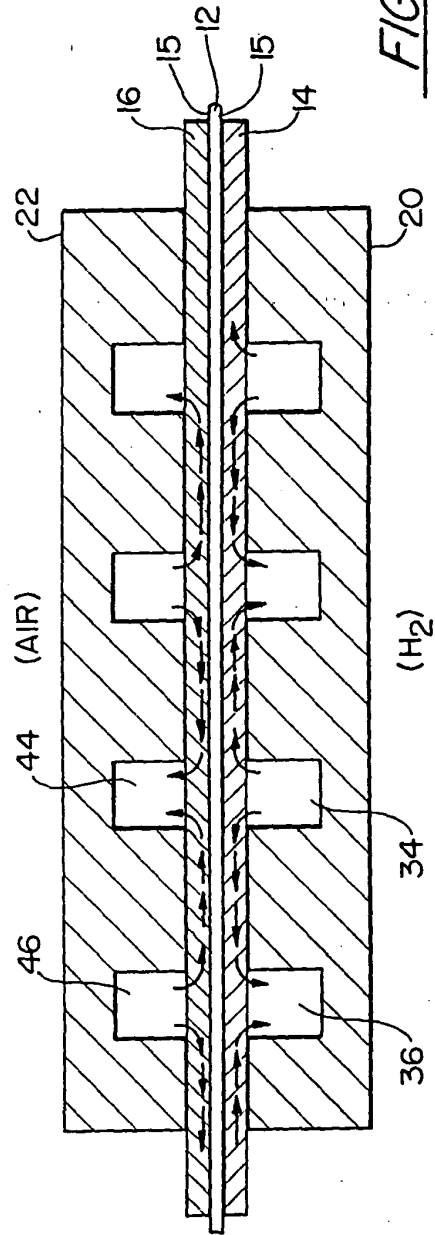


FIG. 2

25. A method as recited in claim 21, wherein said fuel and oxidant flow field channels are noncontiguous and interdigitated, and the step of communicating further comprises communicating the fuel and oxidant reactants from fuel and oxidant inlet channel lengths, through the respective fuel and oxidant diffusion layers, to fuel and oxidant outlet channel lengths, respectively.

26. A method as recited in claim 25, further comprising, prior to the step of exhausting, the step of directing at least one of said reactants through a membrane hydration enhancement zone.

27. A method as recited in claim 26, wherein said reactants are communicated in countercurrent directions through said fuel and oxidant flow field channels.

28. A method as recited in claim 21, further comprising, before the step of introducing, the step of pre-hydrating the membrane.

29. A method as recited in claim 28, wherein said step of pre-hydrating comprises introducing at least one saturated reactant into said fuel cell.

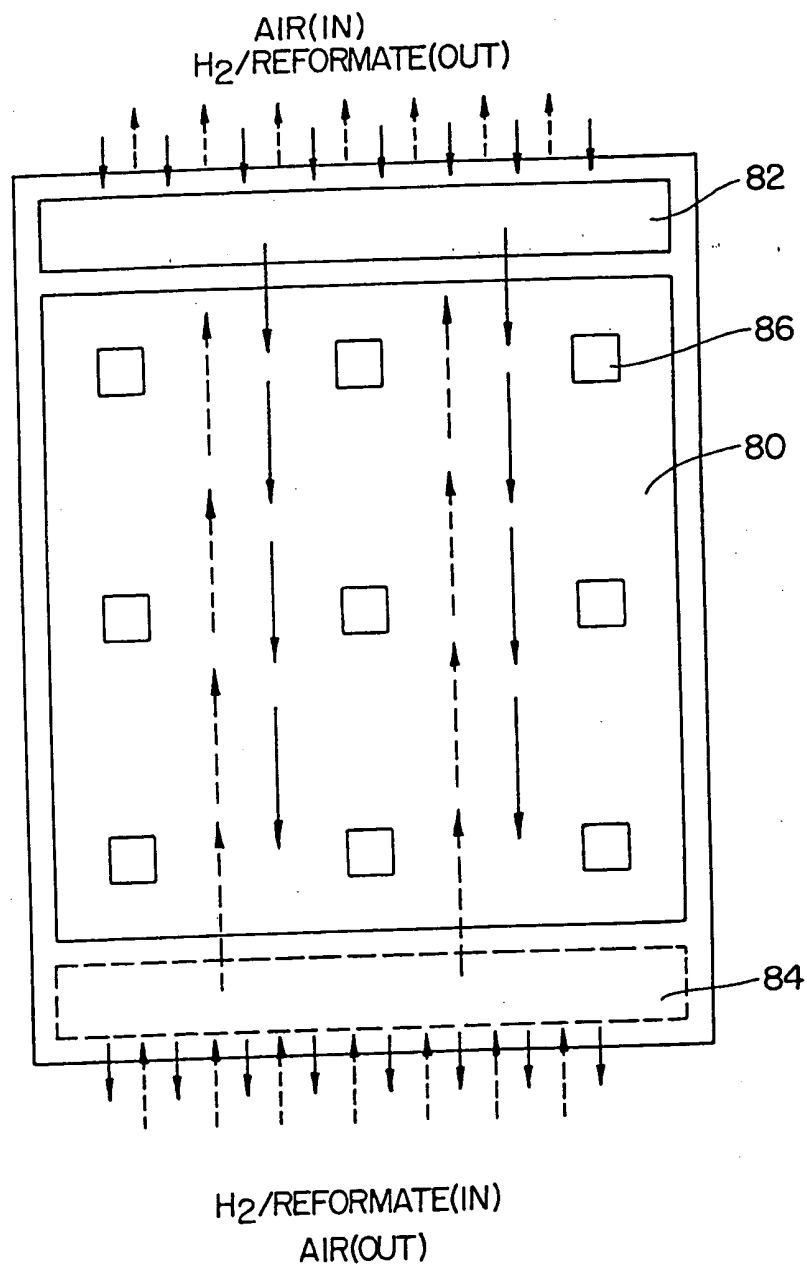


FIG. 5

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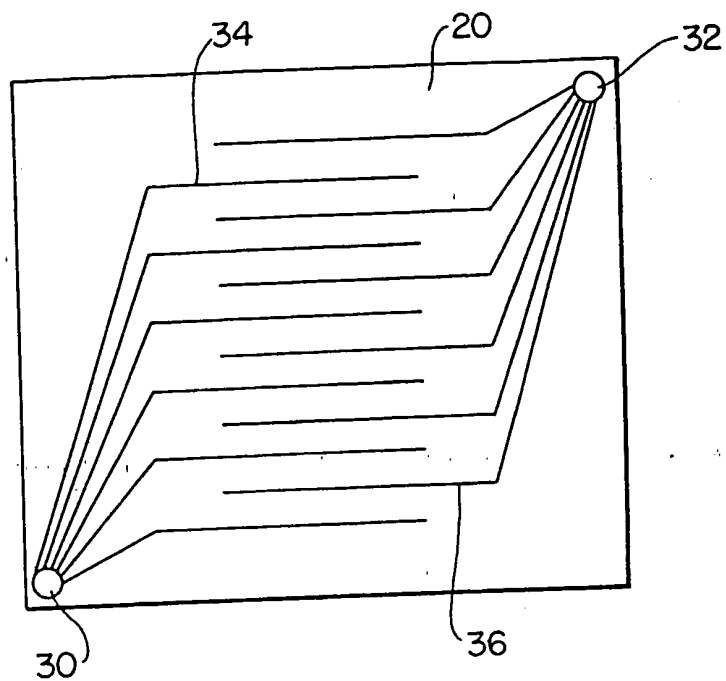


FIG. 3

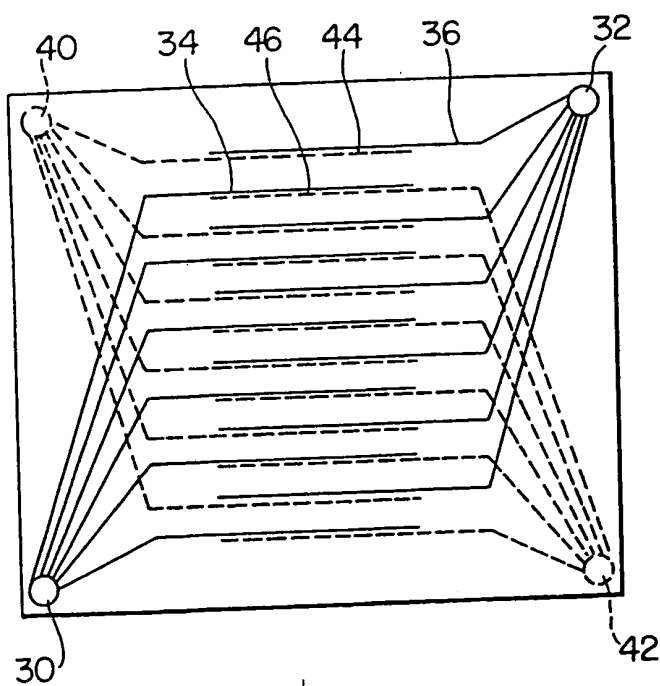


FIG. 4

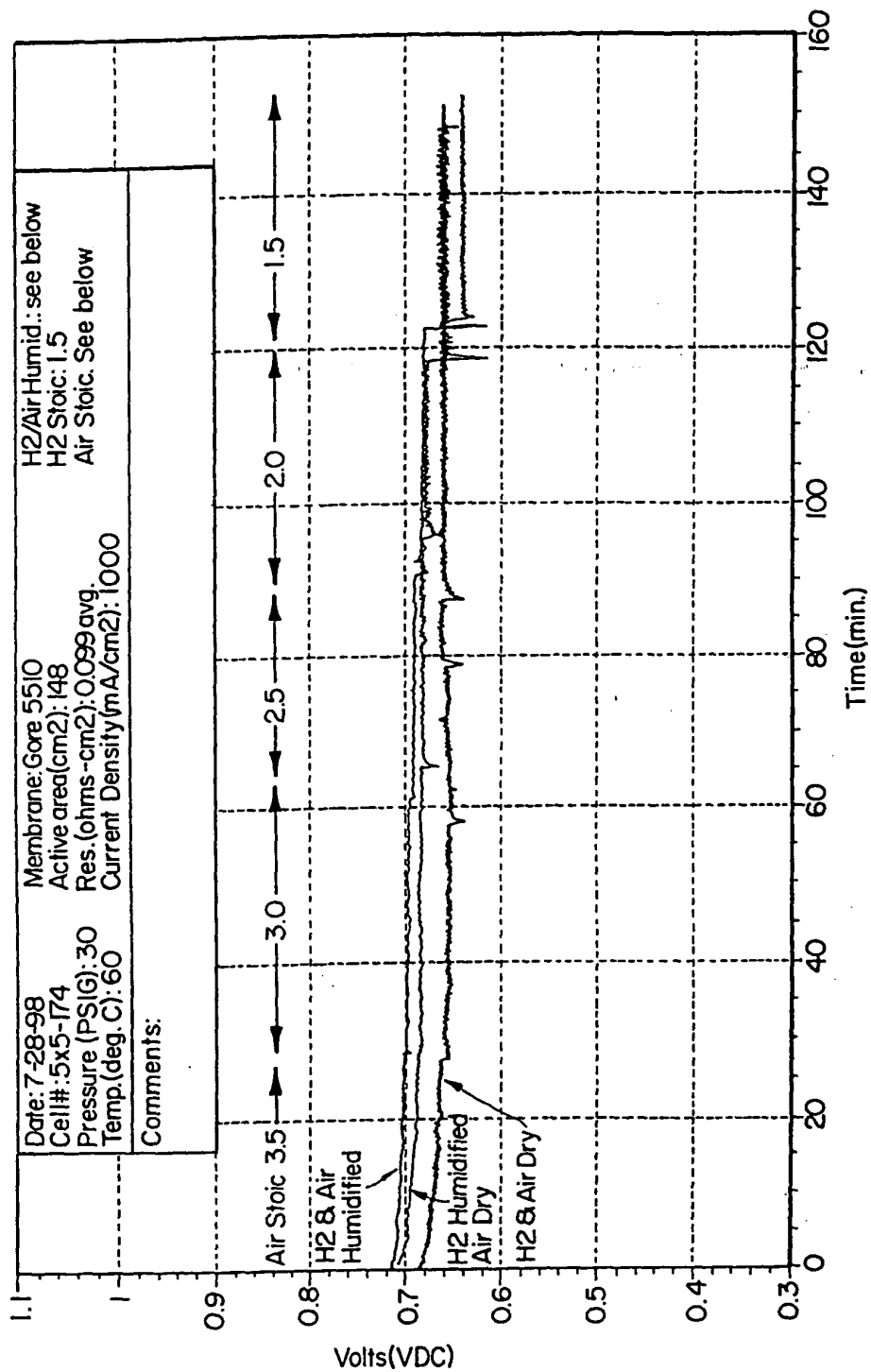
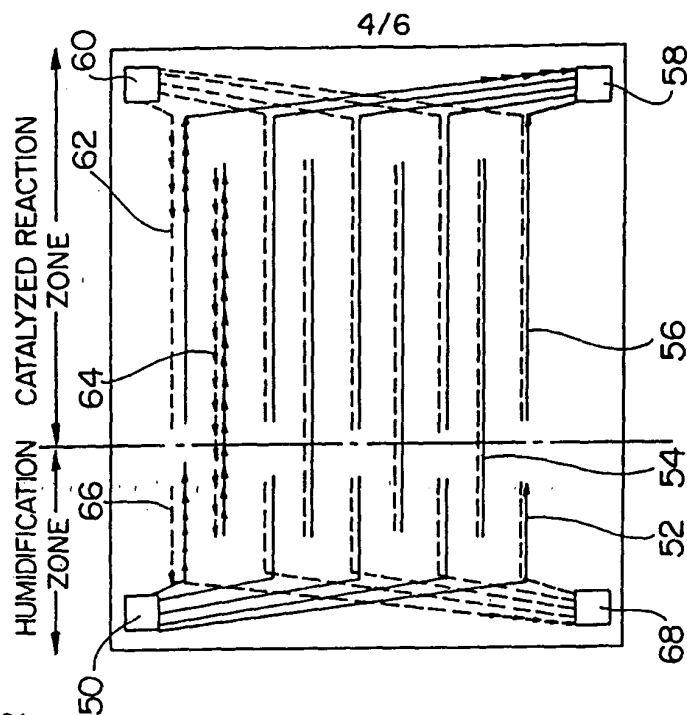
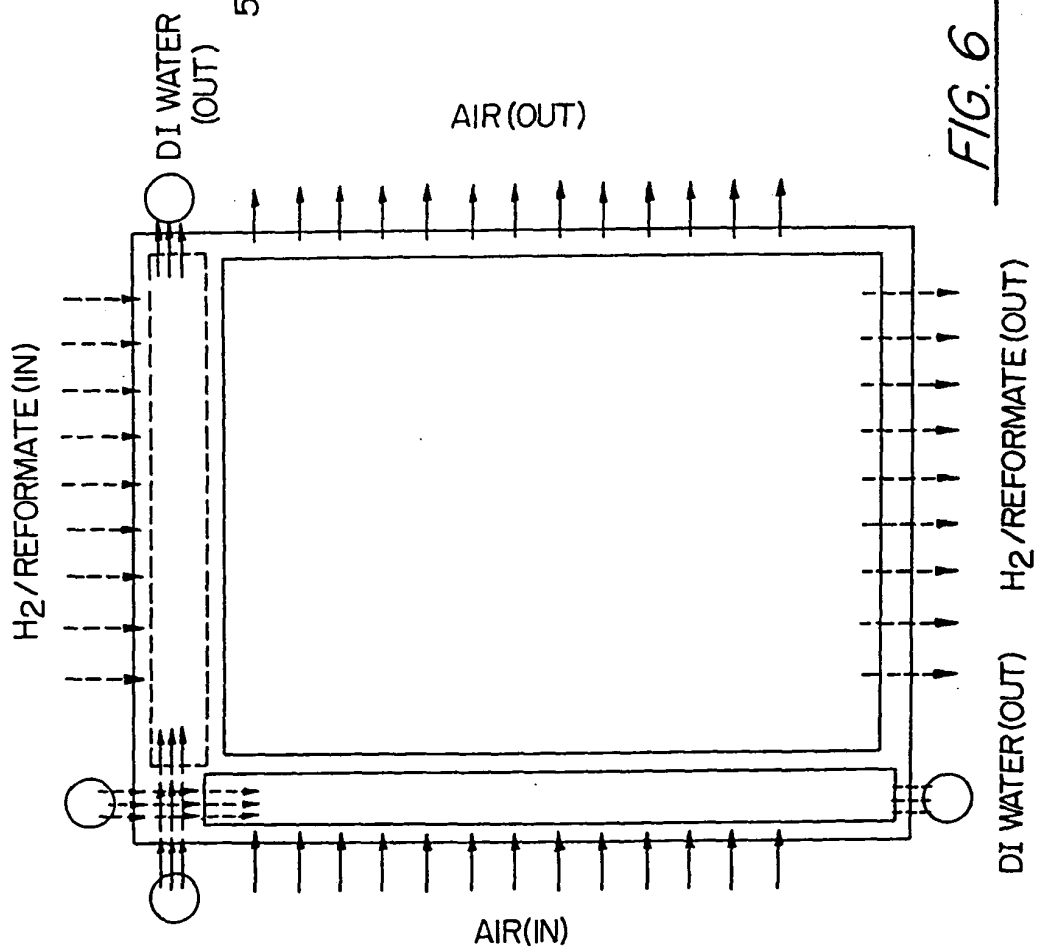


FIG. 8



INTERNATIONAL SEARCH REPORT

International application No.
PCT/JS99/21411

C (Continuation). DOCUMENTS CONSIDERED TO BE RELEVANT		
Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
Y, P	US 5,952,119 A (WILSON) 14 September 1999, col. 3, lines 1-10.	8
A	US 5,641,586 A (WILSON) 24 June 1997, col. 3, line 58 to col. 4, line 7, Fig. 2.	2, 19, 20